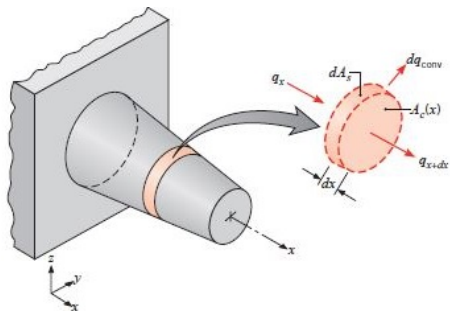
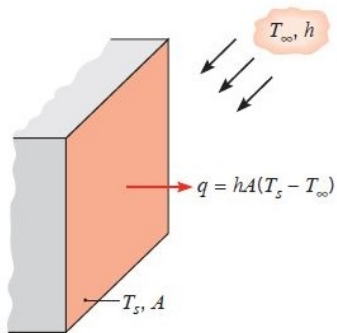


Heat Transfer from Extended Surfaces

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Why Extended Surface?



Analysis of heat transfer from extended surface

Assumptions:

- ▶ One dimensional;
- ▶ Steady state;
- ▶ Constant thermal; conductivity, $k = \text{constant}$;
- ▶ Radiation from surface is negligible;
- ▶ No internal heat generation;
- ▶ h is uniform over the surface;

Energy balance at the differential element:

$$\begin{pmatrix} \text{Rate of Heat} \\ \text{Conduction into} \\ \text{the element at } x \end{pmatrix} = \begin{pmatrix} \text{Rate of heat} \\ \text{conduction from} \\ \text{the element at } x+dx \end{pmatrix} + \begin{pmatrix} \text{Rate of heat} \\ \text{convection} \\ \text{from the element} \end{pmatrix}$$

$$\Rightarrow q_x = q_{x+dx} + dq_{conv} \quad (1)$$

Analysis of heat transfer from extended surface

From Fourier's law,

$$\text{Heat conduction rate at } x, q_x = -KA_c \frac{dT}{dx} \quad (2)$$

Where, A_c = Cross Sectional Area, = $f(x)$

$$\text{Heat conduction rate at } x + dx, q_{x+dx} = q_x + \frac{dq_x}{dx} dx \quad (3)$$

(Truncated Taylor series expansion)

$$\Rightarrow q_{x+dx} = -KA_c \frac{dT}{dx} - K \frac{d}{dx} \left(A_c \frac{dT}{dx} \right) dx \quad (4)$$

$$\text{Convection heat transfer rate, } dq_{conv} = h dA_s (T - T_\infty) \quad (5)$$

Where, A_s = Surface area of the element.

Analysis of heat transfer from extended surface

$$\Rightarrow \frac{d}{dx} \left(A_c \frac{dT}{dx} \right) - \frac{h}{k} \frac{dA_s}{dx} (T - T_\infty) = 0 \quad (6)$$

$$\Rightarrow \frac{d^2 T}{dx^2} + \frac{1}{A_c} \frac{dA_c}{dx} \frac{dT}{dx} - \left(\frac{1}{A_c} \frac{h}{k} \frac{dA_s}{dx} \right) (T - T_\infty) = 0 \quad (7)$$

Let's assume the cross sectional area is uniform, $A_c \neq f(x)$

$$A_s = P x, P = \text{fin perimeter}$$

\Rightarrow

$$dA_s = P dx$$

$$\frac{d^2 T}{dx^2} - \frac{h P}{k A_c} (T - T_\infty) = 0 \quad (8)$$

Further simplify this equation by defining an excess temperature,

$$\theta(x) = T(x) - T_\infty \quad (9)$$

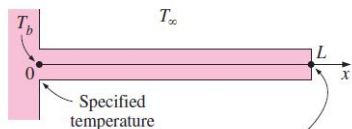
Analysis of heat transfer from extended surface

$$\text{Let's assume, } m^2 = \frac{h P}{k A_c} \quad (10)$$

$$\Rightarrow \frac{d^2\theta}{dx^2} - m^2\theta = 0 \quad (11)$$

It's a linear, homogeneous, second-order differential equation with constant coefficients. Its general solution is of the form,

$$\theta(x) = C_1 e^{mx} + C_2 e^{-mx} \quad (12)$$



- (a) Specified temperature
- (b) Negligible heat loss
- (c) Convection
- (d) Convection and radiation

Thank You